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CLAIMS:

We claim:

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1. A process for the preparation and purification of protein(s) such as viral antigenic proteins, other recombinant therapeutic proteins characterized in that the purification is carried out by a novel technique termed as HIMAX technology which is as herein described and recovering the said protein(s).

- 2. The process as claimed in claim 1 wherein the said protein(s) is/are made to be expressed in the vectors like prokaryotic cell or eukaryotic cell like E.Coli, yeast, etc.
- 3. The process as claimed in the preceding claims wherein the said process and purification comprising-
 - (a) the vector cells are subjected to lysis in the absence of a detergent to obtain a cell lysate;
 - (b) subjecting the cell lysate of steps as to centrifugation ranging from 1000g to 10,000g;
 - (c) obtaining a solid from step(b) by decantation wherein the said solid comprising the said proteins;
 - (d) suspending the said solid in a buffer of pH 6 to 7.5 and optimally treating this with a detergent such as herein described to solubulize the minute impurities if any;
 - (e) as a part of HIMAX technology, the said protein(s) is/are captured by the addition of divalent ionic salt having concentration ranging from 0.2% to 10% with counter ions of either phosphate, chloride and/or acetate solution to form an insoluble matrix;

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(f) subjecting the said insoluble matrix for centrifugation optimally to form pellets;

- (g) subjecting repeated desorptions process to release the bound antigen from insoluble matrix/pellets by using either Tris buffer of Ph 8.0 to 8.5 or Tris buffer with EDTA at Ph 7.0 to 8.0;
- (h) finally recovering the said proteins through ultrafiltration, chromatography on colloidal silica, hydrophobic and or affinity chromatography, ion exchange, diafiltration, sterile filtration or a combination thereof.
- 4. The process as claimed in any of the preceding claims wherein the said protein is a viral antigen,
 - 5. The process as claimed in claim 4 wherein inactivation of viral antigens is carried out by a known manner before subjecting to desorption (by chromatography) step.
- 6. The process as claimed in claims 1 to 3 wherein the said protein is other than viral antigen.
 - 7. The process as claimed in claim 6 wherein inactivation step is avoided before desorption.
- 8. The process as claimed in the preceding claims wherein the chromotographically purified fractions containing the desired protein(s) are pooled for diafiltration and or for sterile filtration.
 - 9. The process as claimed in the preceding claims wherein the divalent cations is preferably Zn, ca, Mg or a combination thereof.
 - 10. The process as claimed in step (d) of claim 3 wherein the detergent is non-ionic detergent.

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11. The process as claimed in step (d) of claim 3 wherein the detergent is not used.

- 12. The process as claimed in step (h) of claim 3 wherein ultra filtration is carried out using membrane filters of 100-300K molecular weight cut off.
- 13. The process as claimed in step (h) of claim 3 wherein the ion-exchange matrices is selected from anionic exchange resins such as sulphated cellulose/DEAE matrices.
 - 14. The process as claimed in the preceding claims wherein the said proteins are highly purified without the loss of biological activity.
- 15. The process as claimed in the preceding claims wherein the contaminants like nucleic acid fragments etc., does not interfere/affect the said process of preparation and purification of the said proteins.
 - 16. The process as claimed in any of the preceding claims wherein viral antigens, recombinant proteins, biotherapeutic proteins etc., are simultaneously prepared and purified.

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